



Internal Corrosion of Crude Oil Pipelines Research at AITF

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Corrosion Engineering
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Outline

- Introduction to Internal Pipeline Corrosion of Crude Oil Pipelines
- Underdeposit Corrosion
 - Inhibitor Evaluation Test Protocol
 - Bacterial Kill Experiments
 - Underdeposit Corrosion Experiments
 - Mechanism
- **P**ipeline **C**orrosion **M**anagement (**PiCoM**) working group
 - Corrosion Monitoring and Underdeposit Corrosion in Pilot Scale Flow Loop
- Summary of Research Direction

Introduction

Internal Pipeline Corrosion when Water-Wet (gathering pipelines)

- Steel wet by oil does not corrode
- Critical water content that will lead to water-wet conditions is generally much greater than 10%
- For corrosion to occur, separation of a water phase from the oil is required
- Internal pitting corrosion models for water-wet conditions



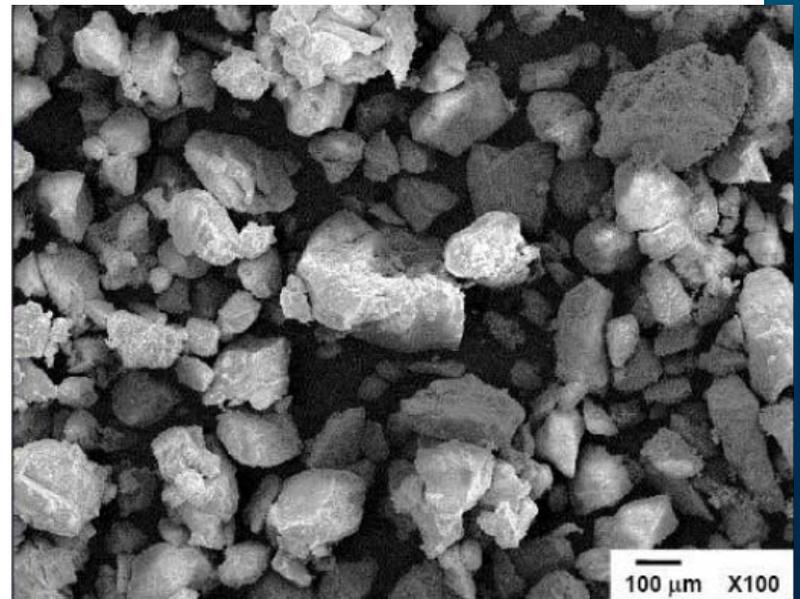
Courtesy of Joe Boivin

Introduction

- Crude oil transmission pipelines (<0.5% BS&W) have a long history without significant corrosion
- 0.5% is usually not a corrosion concern unless conditions exist that enable the precipitation of water on the pipe wall
- Solubility of water in oil only 50-100 ppm
- Water is present as an emulsion, droplets <10 microns, carry chlorides and solids
- Water emulsion droplets are stabilized by asphaltenes and ultrafine submicron clay particles
- Speculation that polar asphaltene flocs can precipitate with water droplets and clay particles, forming larger 100 – 1000 micron clusters

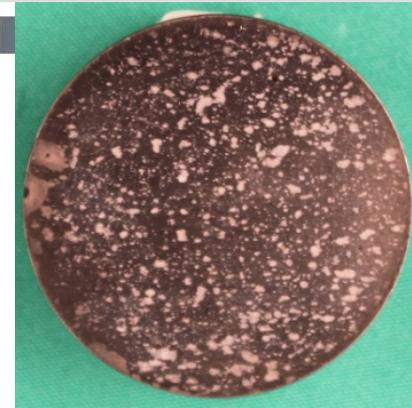
Introduction

- Precipitation at low flow conditions to form sludge in low pressure areas
- Most solids are fine at <44 microns, some are >400 microns and consist primarily of silica sand and iron compounds
- Sludge deposits are mixtures of hydrocarbons, sand, clays, corrosion by-products, bacteria, salts, and water
- Deposits may be layered resulting in variability within the sludge



Underdeposit Corrosion

- Corrosive water film can form on the pipe wall containing salts, chlorides, and organic acids
- Sludges can contain large bacterial populations (SRB, APB, HAB)
- Sludges with waxy oil can exhibit low or no corrosion
- No corrosion observed in the absence of sludge



Sludge covered sample exposed to crude oil for 4 weeks



Bare sample exposed to crude oil for 4 weeks

Sludge Composition

| | | X | Y | Phase I | Phase II |
|-------------------------------|-------------|------|------|---------|----------|
| Soluble in: (wt %) | Heptane | 17.8 | 17 | 15 | - |
| | Xylene | 1.3 | 1.1 | 6.4 | - |
| | Water | 0.8 | 0.4 | 0.7 | - |
| | Acetic acid | 1 | 0.3 | 8.3 | - |
| | HCl | 0.8 | 1.8 | 23.3 | - |
| | Residue | 78.3 | 79.4 | 46.5 | - |
| EDX (wt %) | C | 6.1 | 5 | 11.6 | 6.6 |
| | O | 54.9 | 49.2 | 37.1 | 46.2 |
| | Si | 31.3 | 30 | 14.4 | 26.9 |
| | S | 0.6 | 1.6 | 6 | 1 |
| | Fe | 3.4 | 10.8 | 27.34 | 14.6 |

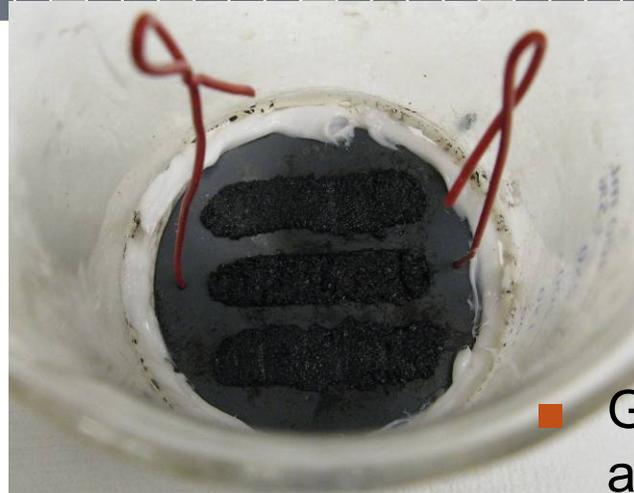
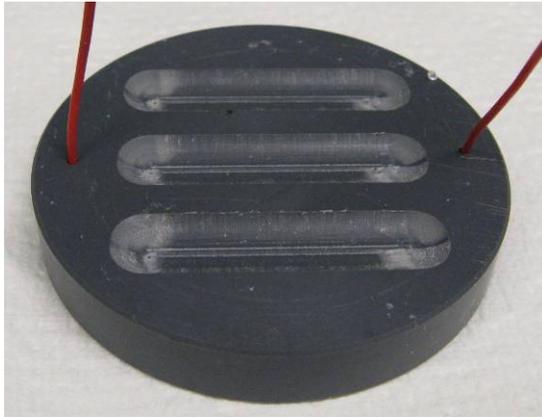
Dean Stark Analysis

| | Phase I | Phase II |
|-------------------------|---------|----------|
| Solid (wt %) | 72.3 | 85 |
| Oil (wt %) | 24.8 | 4.5 |
| Water (wt %) | 2.9 | 10.4 |

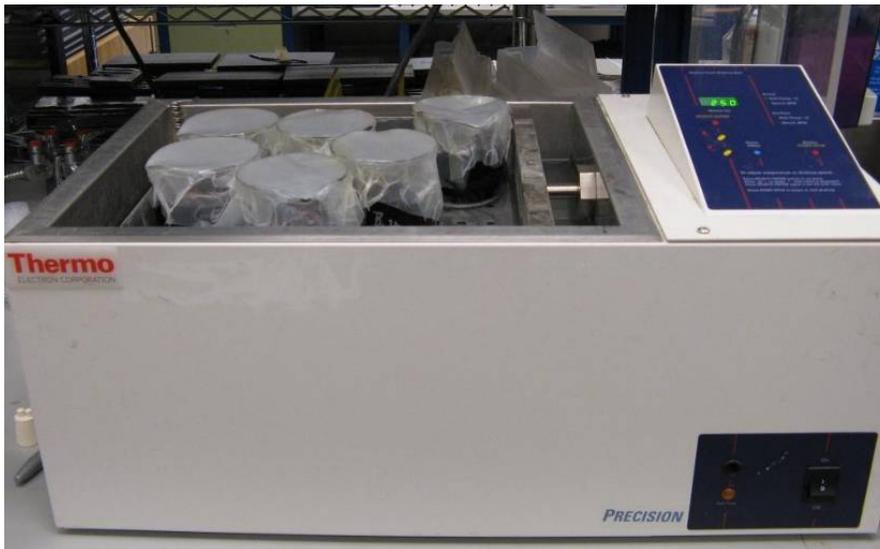
Inhibitor Test Protocol

- Mitigation includes pigging and chemical treatment
- Need to understand the corrosive influence of sediment and the effectiveness of mitigation
- Five chemical inhibitor vendors were encouraged to develop chemical treatments aimed at reducing underdeposit corrosion
- Inhibitor test protocol was developed in collaboration, considering a multifunctional batch inhibitor:
 - Ability to penetrate sludge
 - Filming effectiveness
 - Bacteriocidal properties
- Testing methodology components of bacterial kill experiments and underdeposit corrosion experiments

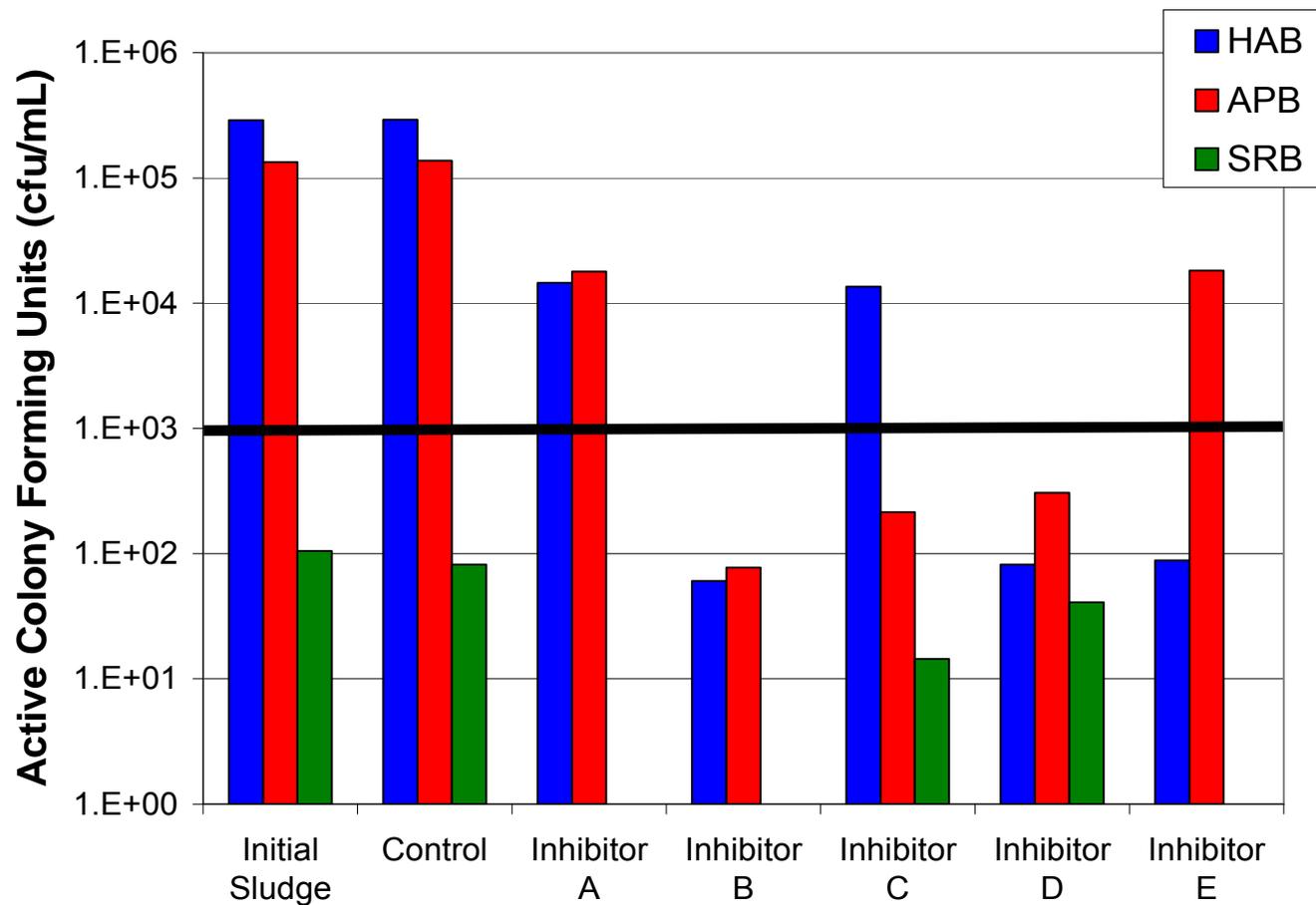
Bacterial Kill Experiments



- Greater surface area for inhibitor penetration
- 2 mm deep sludge
- Oil + 5000 ppm of inhibitor under N_2
- Placed on rocking table for 24 h



Bacterial Kill Experiments



- Sludge with low SRB population
- Inhibitor effectiveness can be measured
- Differences in inhibitor effectiveness are observed

Bacterial Kill Experiments

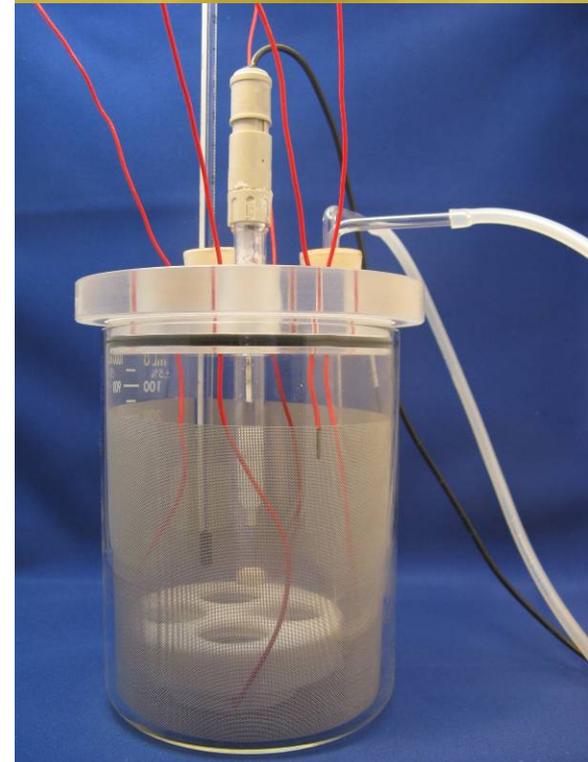
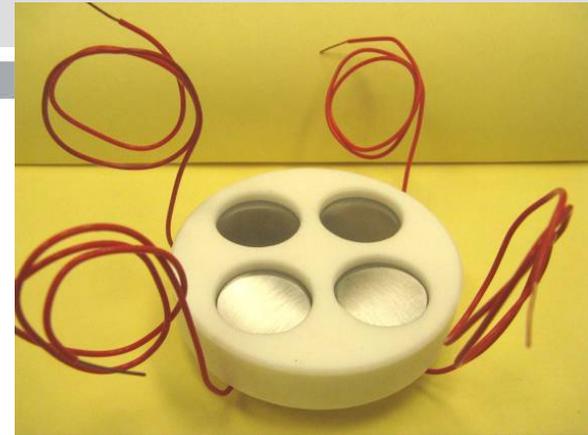
- Methodology may be appropriate, but how well does the inhibitor assessment predict its performance in the field?
 - Complex system
 - Variable oil chemistry
 - Variable sludge chemistry; heterogeneous
 - Bacteria populations are a function of time

Underdeposit Corrosion Testing

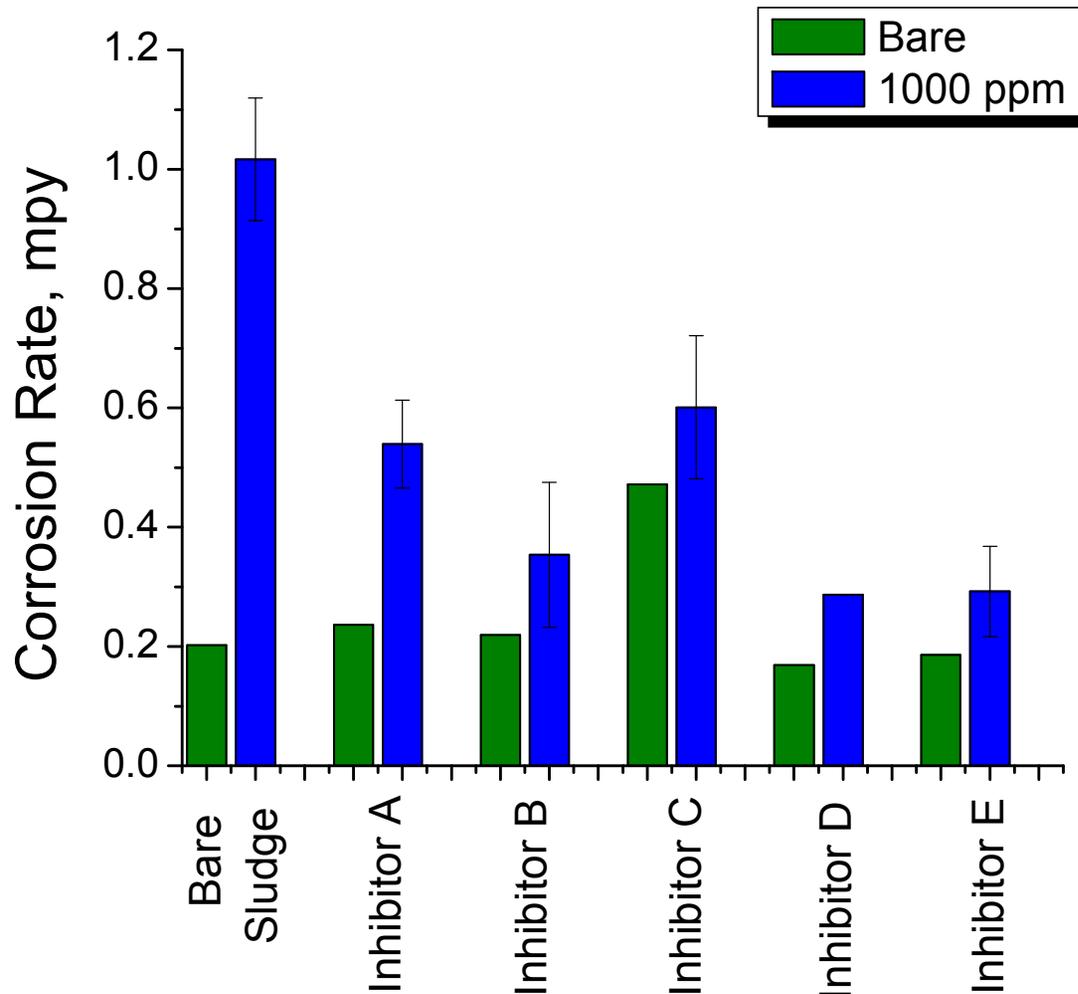
- No standardized underdeposit test procedure
- Oil free sand or oil wetted sand has been used in brine solutions
- Nature of sludge is critical in evaluating the success of an inhibitor
- The test method should be able to assess the inhibitor effectiveness at conditions that can be extended to the pipeline

Underdeposit Corrosion Experiments

- CS coupon, recessed in Teflon holder by 1 mm
- 1 mm thick layer of sludge
- Inhibitor added to the oil
- Controls with no inhibitor
- Pipeline heavy crude oil
- 4-week long exposure experiment on rocking table in anaerobic chamber
- 10% CO₂ / N₂; 25 C
- Visually examined for pits and corrosion and using an optical profiler
- BART before and after



Underdeposit Corrosion Experiments



- 1 mm sludge deposit
- 1000 ppm inhibitor added to oil
- Inhibitors provide protection
- Ability to assess inhibitor performance possible

Underdeposit Corrosion Testing

- The developed methodology enables assessment of inhibitor performance
- Remaining challenges:
 - Variable and dynamic sludge properties
 - Uncertain what the controlling corrosion mechanism is (bacterial corrosion, aqueous corrosion, or combination):
 - Long term corrosion exposure experiments
 - Correlating the corrosion results to the sludge chemistry and bacterial populations

Internal Corrosion of Crude Oil Transmission Lines

Underdeposit corrosion

- Questions remain on:
 - the controlling corrosion parameters
 - the sludge deposition mechanism
 - **the role of crude oil chemistry**
 - **the role of delivery process steps**
- There are crude oil lines that have operated trouble-free for over 25 years
- Not unique to dilbit lines
 - BP experienced leaks in Trans-Alaska pipeline attributed to underdeposit corrosion in the presence of CO₂ and bacterial populations



Trans-Alaska pipeline systems, The Guardian, Jan 2011

PiCoM

PiCoM

PIPELINE CORROSION
MANAGEMENT

- The **Pipeline Corrosion Management** (PiCoM) program at AITF is directed by an Industry Working Group addressing issues of pipeline corrosion and integrity management
- Supported by Alberta government (AET & AITF) and GE Water and Process Technologies
- As of April 2013, the PiCoM program will be an R&D consortium managed by AITF and directed by the operating industry members



Current PiCoM Research

- Directed towards internal Corrosion Monitoring & Mitigation of crude oil pipelines
 - Corrosion underneath sludge deposits (water, MIC)
 - for base-lining and optimization of mitigation tools
- Laboratory experiments evaluating monitoring technologies and mitigation effectiveness
- Design, construction, and commissioning of pilot scale flow loop



Crude Oil Flow Loop

- Crude oil pipeline simulation
- Flow rate and Temperature controlled
- Pig design evaluation
- Chemical inhibitor evaluation
- Real time corrosion rate monitoring
- Simulation of localized corrosion (pitting and MIC)

Crude Oil Flow Loop



Project Proposals

- Effectiveness of Corrosion Inhibitor in Simulated Crude Oil Transmission Pipelines (0.5% BS&W)
- Assessment of the Corrosivity of Sludge from Dilbit Lines versus Sludge from Conventional Crude Oil Lines
- Effectiveness of Corrosion Inhibitor in Simulated Upstream Pipelines (higher water cut)
- Effect of Flow rate on Corrosion in Crude/Water Systems
- Evaluation of Pig Design for Sludge Removal from Corrosion Pits in Heavy Oil Pipelines
- The Effect of Cleaning Pigs on Corrosion Rates when Applied after Inhibitor Filming
- Scoping Study/Survey of Pipe Manufactures and Pipeline Operators with respect to Mill Defects and Solutions to Off-Spec Pipe
- Scoping Study/Literature Review of Life Cycle Analysis for New Non-Metallic Pipeline Materials

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